

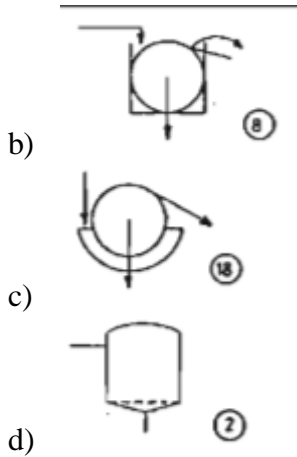
## B. E. Chemical Part I (Sem- VII)

### Chemical Process Design (MCQs)

- 1) Which may not be the part of P & I diagram ---
  - a) Process Equipment
  - b) Off site facilities
  - c) Instruments
  - d) Piping
  
- 2) Locally mounted means controller and display are located in the ---
  - a) Control Room
  - b) Utility section
  - c) Safety office
  - d) Field
  
- 3) QRC is recording controller for ---
  - a) Quality
  - b) Quantity
  - c) Quantum
  - d) Quite
  
- 4) NRE is used to prevent ---- of fluid in pipe line
  - a) Flow
  - b) Pressure
  - c) Back flow
  - d) Velocity
  
- 5) In a double pipe (concentric) heat exchanger, the hydraulic radius for heat transfer (for a fluid flowing through the annulus) would be
  - a) Same as that for fluid flow
  - b) Less than that for fluid flow
  - c) More than that for fluid flow
  - d)  $D_2 - D_1$  ( $D_1$  and  $D_2$  are I.D. of inner and outer pipes respt.)
  
- 6) \_\_\_\_\_ is not a symbol of rotary vacuum filter.



a)






7) The following symbol represents \_\_\_\_\_.

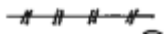


- a. Double Pipe Heat Exchanger
- b. Kettle type Heat Exchanger
- c. Condenser
- d. None of these

8) Identify the Butterfly Valve \_\_\_\_\_

- a. 
- b. 
- c. 
- d. None of the above

9) The following symbol represent \_\_\_\_\_



- a. Electrical Line
- b. Capillary Line
- c. Pneumatic Line
- d. None of the above

10) Discharge of a centrifugal pump is proportional to .....

- A. Impeller diameter(D)
- B.  $D^2$
- C.  $D^3$
- D.  $1/D^3$

- 11) Installing larger diameter pipe in pumping system results in reduction in
- a. Static head
  - b. Frictional head
  - c. Both a and b
  - d. None of the above

- 12) For small discharge at high-pressure following pump is preferred .....

- A. Centrifugal
- B. Axial flow
- C. Propeller
- D. Reciprocating

- 13) Which of the following is not a rotary pump .....

- A. Gear
- B. Vane
- C. Screw
- D. Axial

- 14) Cornell's Equation is,

- a.  $H_G = 0.011 \psi_h (Sc)_v^{0.5} \left( \frac{Dc}{0.305} \right)^{1.11} \left( \frac{Z}{3.05} \right)^{0.33} / (L_w^* f_1 f_2 f_3)^{0.5}$
- b.  $H_G = 0.011 \psi_h (Sc)_v^{0.5} \left( \frac{Dc}{0.305} \right)^{1.11} \left( \frac{Z}{3.05} \right)^{0.33} / (L_w^* f_1 f_2 f_3)$
- c.  $H_G = 0.011 \psi_h (Sc)_v \left( \frac{Dc}{0.305} \right)^{1.11} \left( \frac{Z}{3.05} \right)^{0.33} / (L_w^* f_1 f_2 f_3)^{0.5}$
- d.  $H_G = 0.011 \psi_h (Sc)_v \left( \frac{Dc}{0.305} \right)^{1.11} \left( \frac{Z}{3.05} \right)^{0.33} / (L_w^* f_1 f_2 f_3)$

- 15) Percentage flooding =

- a.  $\left[ \frac{K_4 \text{ at design pressure drop}}{K_4 \text{ at flooding}} \right]^{0.5}$
- b.  $\left[ \frac{K_4 \text{ at design pressure drop}}{K_4 \text{ at flooding}} \right]$
- c.  $\left[ \frac{K_4 \text{ at flooding}}{K_4 \text{ at design pressure drop}} \right]^{0.5}$
- d. None of the above

- 16) Which method can be used to Design of distillation column?

- a. Onda's method
- b. Cornell's method
- c. Both

d. None of the these

17) In a double pipe heat exchanger, in the inner side fluid enters at 20°C and leaves at 45°C. The annulus has steam condensing at 1atm. What is the value of LMTD?

- a) 39°C
- b) 66.7°C
- c) 70°C
- d) 40.5°C

18) Consider we have a Double pipe Heat Exchanger, with inner tube of diameter 20mm (neglect thickness) and outer tube of diameter 30mm. We have two fluids A & B ( $K_A = 15\text{W/mK}$  and  $K_B = 20\text{W/mK}$ ) we desire to have their flow rates as  $15\text{m}^3/\text{s}$  and  $21\text{m}^3/\text{s}$  respectively. If their Nusselt number after calculation is  $\text{Nu}_i = 429$  and  $\text{Nu}_o = 530$ . What is the overall heat transfer coefficient of the equipment is no fouling exists?

- a)  $168.4\text{ W/m}^2\text{K}$
- b)  $168.4 \times 10^3\text{ KW/m}^2\text{K}$
- c)  $188.4\text{ W/m}^2\text{K}$
- d)  $168.4\text{ KW/m}^2\text{K}$

19) Which of the following is not a subset of the category of Tubular Heat Exchangers?

- a) Double pipe
- b) Finned pipe
- c) Shell and Tube
- d) Spiral tube

20) In a double pipe concentric heat exchanger, the equivalent diameter of annulus for heat transfer would be

- a.  $D_2^2 - D_1^2 / D_1$
- b.  $D_2 - D_1$
- c.  $D_2^2 - D_1^2 / D_2$
- d. None of these

21) Which is the major mean of heat transfer in a Double Pipe heat exchanger?

- a) Convection
- b) Conduction
- c) Radiation
- d) Combined Convection and Conduction

- 22) Fouling factor must be included in the calculation of overall design heat transfer coefficient, when the liquid
- containing suspended solids flows at low velocity.
  - containing suspended solids flows at high velocity.
  - is highly viscous.
  - is of high specific gravity.
- 23) Which of the following has the maximum Log mean temperature difference for a Double Pipe Heat Exchanger?
- Counter-flow
  - Parallel Flow
  - Cross Flow
  - Split Flow
- 24) Hydraulic gradient line (H.G.L.) represents the sum of .....
- Pressure head and kinetic head
  - Kinetic head and datum head
  - Pressure head and datum head
  - Pressure head, kinetic head and datum head
- 25) The density of the fluids, its viscosity and the thermal conductivity (K) is measured at \_\_\_\_\_
- LMTD
  - Mean temperature
  - Median of the temperature
  - Square mean of the temperature
- 26) The pressure drop required across a control valve will be a function of -----
- Pressure in line
  - Valve design
  - Density of flowing material
  - Viscosity of flowing material
- 27) If  $T_1 = 390^\circ F$ ,  $T_2 = 200^\circ F$ ,  $t_1 = 100^\circ F$ ,  $t_2 = 170^\circ F$  then  $R = \underline{\hspace{1cm}}$ ,  $S = \underline{\hspace{1cm}}$
- 2.70, 0.245
  - 2.75, 0.241
  - 2.71, 0.241
  - 2.71, 0.245
- 28) If  $T_1 = 390^\circ F$ ,  $T_2 = 200^\circ F$ ,  $t_1 = 100^\circ F$ ,  $t_2 = 170^\circ F$  Then LMTP (Counter Current) = \_\_\_\_\_  $^\circ F$
- $152.8^\circ F$
  - $153.3^\circ F$
  - $151.2^\circ F$
  - $152.2^\circ F$

- 29) IF  $W=12400$  lb/hr,  $\lambda= 961$  Btu/lb,  $U= 250$  Btu/hr. $ft^2$ .  $^{\circ}F$  ,  
 $T_1= 224$   $^{\circ}F$   $T_2=194$   $^{\circ}F$  then area 'A' = \_\_\_\_\_
- a)  $1585ft^2$       b)  $1595ft^2$       c)  $1580ft^2$       d)  $1590ft^2$
- 30) lb of water evaporated divided by lb of steam is called as \_\_\_\_\_ economy.
- a) Water      b) Steam      c) Process      d) Evaporator
- 31) The shortest distance between two adjacent tube holes is called as
- a) Square pitch      b) Gap between the tubes  
c) Clearance      d) Pitch
- 32) Which is not the essential constituent of streams in the flow sheet
- a) Temperature      b) Flow rates  
c) Physical Properties      d) Compositions
- 33) Computer aided flow sheeting are capable of producing\_\_\_\_\_ .
- a) Accurate and detailed material balance  
b) Preliminary equipment design  
c) Rigorous simulator heat & material balance  
d) All the above
- 34) ISO means in coding system\_\_\_\_\_.
- a) International Standardization Organization  
b) Organization of International Standards  
c) International Organization of Standard  
d) International organization for standardization
- 35) Standard Inlet velocity of dust, laden gas in cyclone separator is\_\_\_\_\_
- a. 5 to 25 m/s  
b. 6 to 26 m/s  
c. 7 to 27 m/s  
d. 9 to 27 m/s

36) If  $D_c = 420$  mm, then Cyclone inlet duct area is \_\_\_\_\_  $\text{mm}^2$ .

- a. 17500
- b. 17600
- c. 17540
- d. 17640

37) At Reynolds's No. = 167. Find the value of  $j^H =$

- a. 120
- b. 167
- c. 267
- d. 67

38) Find the specific heat of Benzene at  $T_{\text{avg}} = 100$   $^{\circ}\text{F}$ .

- a. 0.425 Btu / (lb)( $^{\circ}\text{F}$ )
- b. 0.665 Btu / (lb)( $^{\circ}\text{F}$ )
- c. 0.113 Btu / (lb)( $^{\circ}\text{F}$ )
- d. 0.005 Btu / (lb)( $^{\circ}\text{F}$ )

39) If  $f_c = 0.005$ ,  $A_s = 2.218 \times 10^6$   $\text{mm}^2$ ,  $A_1 = 16800$   $\text{mm}^2$ , then  $\psi =$  \_\_\_\_\_.

- a. 0.55
- b. 0.60
- c. 0.66
- d. 0.77

40) In a reactor if  $E = 19 \times 10^7$   $\text{Kg}/\text{mm}^2$ ,  $t = 6.045$  mm,  $D_o = 8368$  mm,  $L = 10570$  mm.

Then critical buckling pressure is \_\_\_\_\_ and allowable pressure is \_\_\_\_\_.

- a. 0.0540  $\text{Kg}/\text{cm}^2$ , 0.0136  $\text{Kg}/\text{cm}^2$
  - b. 0.1540  $\text{Kg}/\text{cm}^2$ , 0.1136  $\text{Kg}/\text{cm}^2$
  - c. 0.4540  $\text{Kg}/\text{cm}^2$ , 0.4136  $\text{Kg}/\text{cm}^2$
  - d. 0.0040  $\text{Kg}/\text{cm}^2$ , 0.0036  $\text{Kg}/\text{cm}^2$
-